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Enhancing the activity and stability of RuO₂-based catalyst *via* nano-confinement effect for O₂ evolution reaction in acid electrolyte

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Abstract

The oxygen evolution reaction (OER), as a pivotal process in electrochemical water splitting, directly determines energy conversion efficiency. Ruthenium (Ru)-based catalysts have gained considerable attention in recent years due to their decent intrinsic activity in acidic media. Previous studies have demonstrated that while Ru exhibits superior OER activity compared to RuO₂ in acidic environments, its operational stability remains markedly inferior. This performance dichotomy, coupled with the persistent challenges of active species dissolution and catalyst particle aggregation during prolonged operation, significantly hinders their practical implementation in electrochemical systems. To address these challenges, this study develops a carbon nanotube (CNT)/Fe-Ni@RuO₂@PANI-350 composite catalyst composed of RuO₂ nanoparticles supported on bimetallic Fe-Ni modified CNTs (CNT/Fe-Ni) and encapsulated with polyaniline (PANI). This catalyst utilizes the anchoring effect of bimetallic Fe-Ni sites and the spatial confinement effect of PANI coating layer, effectively inhibiting the dissolution and agglomeration of RuO₂ during both high-temperature processing and electrochemical operation, thereby



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significantly enhancing electrochemical stability. The anchoring strength of RuO₂ nanoparticles on CNT/Fe-Ni support *via* the nano-confinement effect, as well as the microscopic mechanisms underlying the performance enhancement, are revealed by density functional theory calculations and experimental characterizations. The composite catalyst demonstrates fascinating OER performance in 0.5 M H₂SO₄, exhibiting a low Tafel slope of 39.1 mV dec⁻¹ as well as low overpotentials of 188 and 225 mV at current densities of 10 and 100 mA cm⁻², respectively. Remarkably, the composite catalyst demonstrates significantly enhanced stability, exhibiting only ~30 mV overpotential increase during 150 h continuous operation at 10 mA cm⁻². This study highlights a simple yet effective nano-confinement strategy to address the challenges of Ru-based catalysts, and provides a practical paradigm for designing and preparing highly efficient OER electrocatalysts with enhanced stability.

Keywords: Oxygen evolution reaction (OER), ruthenium (Ru)-based catalysts, nano-confinement strategy, electrochemical stability

INTRODUCTION

Electrochemical water splitting is recognized as one of the most promising methods for producing H₂, which is considered perhaps the ultimate sustainable and clean energy resource in modern society^[1,2]. Electrochemical water splitting comprises the hydrogen evolution reaction (HER) at the cathode and the oxygen evolution reaction (OER) at the anode. Compared to HER, OER exhibits sluggish kinetics due to its complex multi-electron and proton transfer processes, making it the rate-determining step in an overall water-electrolysis process^[3-5]. The high overpotentials required for OER, particularly in acidic electrolytes, and the poor stability of electrocatalysts further hinder its practical applications^[6,7]. Thus, developing high-performance OER electrocatalysts in acidic environment remains challenging. In previous studies on OER catalysts, Ruthenium (Ru)-based catalysts have attracted much attention due to their relatively high activity in acidic media^[8].

However, Ru-based catalysts are facing significant challenges including high cost, particle aggregation at elevated temperature during preparation, poor electrochemical stability^[9-14], particularly under strong oxidizing conditions or exposed acidic electrolytes where the dissolution of Ru species leads to active site loss and rapid performance degradation^[15-17]. Among these challenges, the dissolution of Ru species is directly related to stability deterioration and lifespan shortening^[18]. To address this challenge, previous studies have proposed various strategies, including metal doping^[19], heterostructure engineering^[20], defect engineering^[21], morphology control^[22], and modifications of catalyst supports^[23]. Generally, the selection of catalyst supports plays a critical role in determining catalytic performance, as they profoundly influence the activity, stability, and electron transfer properties^[24-27]. Carbon-based materials, particularly carbon nanotubes (CNTs), have emerged as prominent candidates in catalyst support research due to their exceptional electrical conductivity, large specific surface area, and superior chemical stability^[28].

In this study, Fe-Ni co-modified CNTs (CNT/Fe-Ni) were designed as the support of Ru-based catalysts, and the catalytic activity and stability of RuO₂ in OER under acidic conditions were investigated. The CNT/Fe-Ni material was synthesized via chemical vapor deposition (CVD), where ferrocene and nickelocene served not only as the catalyst for CNT growth but also as precursors to *in situ* form the Fe-Ni anchor sites for subsequent RuO₂ growth *via* nano-confinement effect. Thereafter, the nanostructure is stabilized by coating with a polyaniline (PANI) layer, to prevent the agglomeration of RuO₂ nanoparticles during the subsequent high-temperature treatment and electrochemical operation. Such a structure design of the composite catalyst leverages the anchoring effect of bimetallic Fe-Ni alloy to facilitate the confined growth of RuO₂ nanoparticles on Fe-Ni alloy sites and establish a strong metal-support interaction. This design not only utilizes the high conductivity and large specific surface area of CNTs, but also optimizes the Ru active

sites through interfacial electronic coupling between Ni, Fe, and Ru, thereby significantly enhancing the catalytic activity and stability of the catalyst during OER process. This study underscores a simple yet effective nano-confinement strategy to address challenges faced by Ru-based catalysts in acidic environments, providing a practical paradigm for designing and preparing highly efficient OER electrocatalysts with enhanced stability.

EXPERIMENTAL

Chemicals and materials

Ferrocene (high purity, $\geq 99.5\%$) was purchased from Alfa Aesar. Nickelocene (analytical grade, $\geq 98.0\%$) was obtained from Macklin. RuCl_3 (analytical grade, $\geq 97.0\%$) was supplied by Ark Pharm. Urea (analytical grade, $\geq 99.0\%$) and ammonium persulfate (APS, analytical grade, $\geq 98.0\%$) were procured from Aladdin. Acetonitrile (analytical grade, $\geq 99.5\%$) was purchased from Sinopharm Chemical Reagent Co., Ltd. Aniline (analytical grade, $\geq 99.0\%$) was obtained from Alfa Aesar, while isopropanol (analytical grade, $\geq 99.7\%$) was supplied by Shanghai Lingfeng Chemical Reagent Co., Ltd. Nafion solution (5%, D520, DuPont) was purchased from Shanghai Hesun Electric Co., Ltd. All chemicals used in this work were employed without further purification.

Preparation of CNT/Fe-Ni support

A total of 50 mg of nickelocene and 50 mg of ferrocene were placed at the low-temperature zone of a tubular furnace, maintaining a constant Ar flow rate of 300 sccm inside the tube. When the furnace temperature reached 850 °C (heating rate: 4 °C min⁻¹), an acetonitrile:ethanol mixture (v/v = 3:1) was heated to 90 °C, and the resulting vapor was introduced into the furnace using an Ar carrier gas. After 5 min of reaction, the product was cooled to obtain CNT/Fe-Ni.

Synthesis of CNT/Fe-Ni@RuO₂-350

A total of 45 mg of CNT/Fe-Ni was dispersed in 42 mL of ethanol, followed by the addition of 45 mL of deionized (DI) water. The mixture was ultrasonicated for 5 min. Under continuous stirring, 3 mL of 0.05 M RuCl_3 solution and 300 mg of urea were added. The homogeneous solution was then transferred into a 150 mL Teflon-lined autoclave and subjected to a hydrothermal reaction at 180 °C for 4 h. After cooling to room temperature, the product was thoroughly washed with water and ethanol via centrifugation and dried in an oven at 55 °C to obtain CNT/Fe-Ni@RuO₂. The dried sample was calcined in a muffle furnace at 350 °C for 4 h (heating rate: 2 °C min⁻¹) to yield the final CNT/Fe-Ni@RuO₂-350 material.

The control samples, CNT/Ni@RuO₂-350 and CNT/Fe@RuO₂-350, were synthesized using 0.1 g of nickelocene and ferrocene, respectively, as catalysts for the preparation of CNT/Ni and CNT/Fe, while the subsequent steps remained unchanged.

Synthesis of CNT/Fe-Ni@RuO₂@PANI-350

A total of 40 mg of CNT/Fe-Ni@RuO₂ was dispersed in 40 mL of DI water via ultrasonication. The resulting mixture was placed in an ice bath, followed by the addition of 10 mL of 0.5 M HCl containing 60 μL of aniline and another 10 mL of 0.5 M HCl containing 120 mg of APS. The reaction system was continuously stirred in an ice bath for 10 h. The obtained product was washed thoroughly with water and ethanol via centrifugation and subsequently dried in an oven at 55 °C. The dried sample was then calcined in a muffle furnace at 350 °C for 4 h (heating rate: 2 °C min⁻¹) to obtain CNT/Fe-Ni@RuO₂@PANI-350.

The control samples, CNT/Ni@RuO₂@PANI-350 and CNT/Fe@RuO₂@PANI-350, were synthesized using 0.1 g of nickelocene and ferrocene, respectively, as catalysts for the preparation of CNT/Ni and CNT/Fe, while the subsequent steps remained unchanged.

Characterization

Powder X-ray diffraction (XRD) patterns were recorded using a Bruker D8 Advance Davinci diffractometer (Germany) with Cu K α radiation ($\lambda = 1.54178 \text{ \AA}$). Surface morphology and elemental composition were analyzed using a field emission scanning electron microscope (SEM, Zeiss Supra55, GER) and a high-resolution transmission electron microscope (HR-TEM, JEM-2100, JEOL, Japan), with corresponding energy-dispersive X-ray spectroscopy (EDS) data collected. X-ray photoelectron spectroscopy (XPS) analysis was performed on an ESCALAB 250Xi spectrometer (Thermo Fisher, USA) with monochromatic Al K α radiation (150 W), calibrated to the C 1s peak at 284.8 eV. Raman spectra were carried out on a Spelec Raman spectrometer with 532 nm laser.

Electrochemical measurements

Electrochemical measurements were conducted using a CHI 760E electrochemical workstation (Shanghai Chenhua Instrument Co., Ltd.). A conventional three-electrode system was employed, with a 3 mm-diameter glassy carbon electrode (GC) as the working electrode, a carbon rod as the counter electrode, and an Ag/AgCl electrode as the reference electrode. The catalyst ink was drop-cast onto the GC electrode and dried under an infrared lamp to prepare the working electrode. Catalyst ink was prepared by dispersing 5.0 mg of catalyst in a 1.0 mL water/isopropanol (3:1, v/v) mixture containing 10.0 μL of 5.0% Nafion solution (Sigma-Aldrich), followed by ultrasonication for 30 min. Prior to catalyst loading, the GC electrode was sequentially polished using 0.1 and 0.03 μm Al $_2$ O $_3$ powder and rinsed with DI water. The catalyst loading was controlled at $\sim 0.35 \text{ mg cm}^{-2}$.

The linear sweep voltammetry (LSV) measurements were conducted at a scan rate of 5.0 mV s $^{-1}$ in an electrolyte of 0.5 M H $_2$ SO $_4$. The potentials measured in the three-electrode system were converted to the corresponding reversible hydrogen electrode (RHE) potentials using the transformation equation: $E_{\text{RHE}} = E_{\text{Ag/AgCl}} + 0.0592 \times \text{pH} + 0.197$. Unless otherwise specified, all data were corrected for 90% IR compensation. The time-potential curve was recorded by maintaining the current density of the working electrode at 10.0 mA cm $^{-2}$. Prior to LSV testing, the catalyst was activated via 20 cycles of cyclic voltammetry (CV) testing.

The electrochemical impedance spectroscopy (EIS) measurements were performed at 1,600 rpm under an applied potential of 1.45 V vs. RHE, within a frequency range of 10 5 -10 $^{-1}$ Hz. The electrochemical double-layer capacitance (C_{dl}) of the catalyst was estimated by measuring at different scan frequencies within the potential range of 1.1-1.2 V vs. RHE. The C_{dl} value was determined from the slope of the linear relationship between the half-difference of the anodic and cathodic current densities ($\Delta j = j_{\text{anode}} - j_{\text{cathode}}$) and the scan rate (ν) at 1.15 V vs. RHE. The electrochemically active surface area (ECSA) of the catalyst was calculated using $\text{ECSA} = C_{\text{dl}} \cdot S / C_s$, where C_s is the roughness factor with a value of 35 $\mu\text{F cm}^{-2}$, and S is the geometric area of the electrode. For long-term time-potential measurements, a carbon paper electrode loaded with the catalyst (mass loading 1.5 mg cm $^{-2}$) was used as the working electrode, with the current density maintained at 10.0 mA cm $^{-2}$.

DFT

The spin-polarized density functional theory (DFT) calculations were performed using the Vienna Ab initio Simulation Package (VASP)^[29-31]. The projector augmented-wave (PAW) method was employed to describe the core-valence electron interactions^[32]. The exchange-correlation interactions were treated within the generalized gradient approximation (GGA) using the Perdew-Burke-Ernzerhof (PBE) functional^[33]. Structural optimizations and static self-consistent calculations were conducted with Gamma-centered 1 \times 1 \times 1 and 3 \times 3 \times 1 k-point meshes, respectively. A plane-wave cutoff energy of 450 eV was adopted. The energy convergence threshold was set to 1 \times 10 $^{-6}$ eV, while the force convergence criterion was 0.02 eV/ \AA . A

vacuum layer of 20 Å was introduced to minimize periodic interactions between adjacent slabs. Long-range van der Waals interactions were accounted for using the DFT-D3 dispersion correction method^[34].

The OER activity of the catalyst was evaluated through the computational hydrogen electrode (CHE) model proposed by Nørskov *et al.*^[35]. This model considers four elementary steps, with the Gibbs free energy change for each step calculated using [which incorporates zero-point energy (ZPE) correction and entropy contribution (TS)]:

$$\Delta G = \Delta E + \Delta ZPE - T\Delta S + \Delta G_U \quad (1)$$

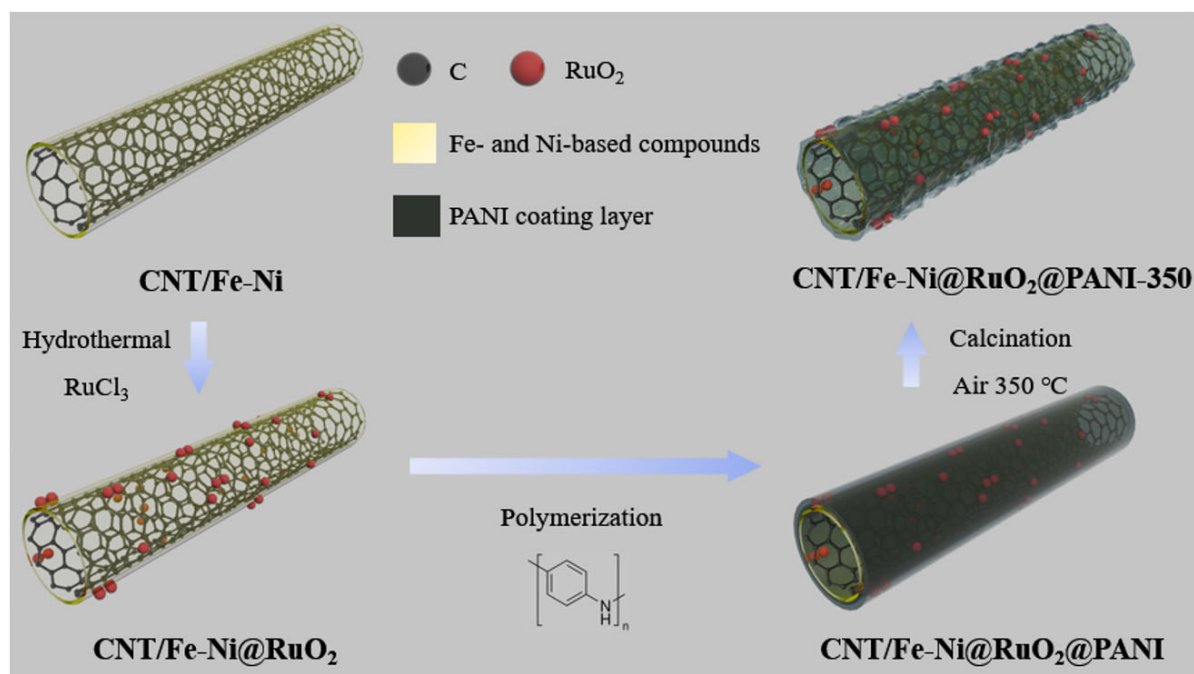
Here, ΔE represents the binding energy change of intermediate species (e.g., *OH, *O, *OOH), and $\Delta G_U = -eU$ (where U denotes the applied electrode potential). Differential charge density analysis and global average differential charge density profiles were obtained using the VASPKIT toolkit^[36].

RESULTS AND DISCUSSION

The Fe-Ni modified CNTs (CNT/Fe-Ni) were synthesized via CVD using a mixed solvent of ethanol and acetonitrile with varying ratios as the carbon source under Ar carrier gas, using both nickelocene and ferrocene as the catalysts for CNT growth. Scanning electron microscopy (SEM) images of the CNT/Fe-Ni samples synthesized with varying volume ratios of ethanol to acetonitrile are shown in [Supplementary Figure 1](#). These CNT/Fe-Ni samples consist of CNTs with varied aspect ratios. Notably, when the volume ratio of ethanol to acetonitrile is 2:3, the CNTs with a uniform diameter of ca. 150 nm (denoted as CNT/Fe-Ni) were obtained [[Supplementary Figure 2](#)]. The RuO₂-decorated CNT/Fe-Ni (denoted as CNT/Fe-Ni@RuO₂) was synthesized *via* a solvothermal reaction using CNT/Fe-Ni and RuCl₃ as precursors. Subsequently, a PANI layer was polymerized on the surface of CNT/Fe-Ni@RuO₂ to form CNT/Fe-Ni@RuO₂@PANI, which was further calcined in air at 350 °C for 4 h to obtain the final CNT/Fe-Ni@RuO₂@PANI-350 catalyst [[Scheme 1](#)].

The structure of CNT/Fe-Ni is first characterized by XRD and XPS. The diffraction peak of graphitic carbon [[Supplementary Figure 3A](#)] could be clearly observed, but the characteristic diffraction peak of Fe-Ni alloy was rather weak, indicating the particle size of the generated Fe-Ni alloy is either too small or highly dispersed in the carbon matrix. In the Fe 2p XPS spectrum [[Supplementary Figure 4](#)], the peaks at binding energies of 707.2, 711.2 and 713.3 eV correspond to Fe⁰, Fe²⁺, and Fe³⁺, respectively, with a satellite peak at 717.8 eV (Fe 2p_{3/2}). Similarly, in the Ni 2p_{3/2} spectrum, the peaks at binding energies of 852.6, 853.8 and 855.0 eV are related to Ni⁰, Ni²⁺, and Ni³⁺, respectively, with a satellite peak at 861.7 eV. The existence of Fe⁰ and Ni⁰ demonstrated that they exist in metallic and/or alloying counterparts, consistent with XRD analysis. The high valence states of Fe (Fe²⁺, Fe³⁺) and Ni (Ni²⁺, Ni³⁺) might result from the surface oxidation of metallic Fe and Ni^[13].

The morphology of CNT/Fe-Ni, CNT/Fe-Ni@RuO₂, CNT/Fe-Ni@RuO₂@PANI and CNT/Fe-Ni@RuO₂@PANI-350 is investigated by transmission electron microscopy (TEM). The representative TEM image of CNT/Fe-Ni [[Figure 1A](#)] displays the nanotube with a diameter of 150 nm. The high-resolution TEM image (insert in [Figure 1A](#)) reveals an average interplanar spacing of 0.345 nm, which is assigned to the (002) crystal plane of graphite, indicating that the CNTs exhibit high crystallinity^[37]. After the hydrothermal reaction at either low or high RuCl₃ concentration, RuO₂ nanoparticles are observed to be anchored on the surface of CNT/Fe-Ni with high uniformity, as shown in [Figure 1B](#), indicating that Fe-Ni on the CNT/Fe-Ni surface is likely to induce a nano-confinement effect for preferentially depositing RuO₂ nanoparticles on the Fe-Ni sites. Such an effect promotes strong metal-support interaction, which is expected to stabilize Ru



Scheme 1. Schematic illustration of the synthesis of CNT/Fe-Ni@RuO₂@PANI-350.

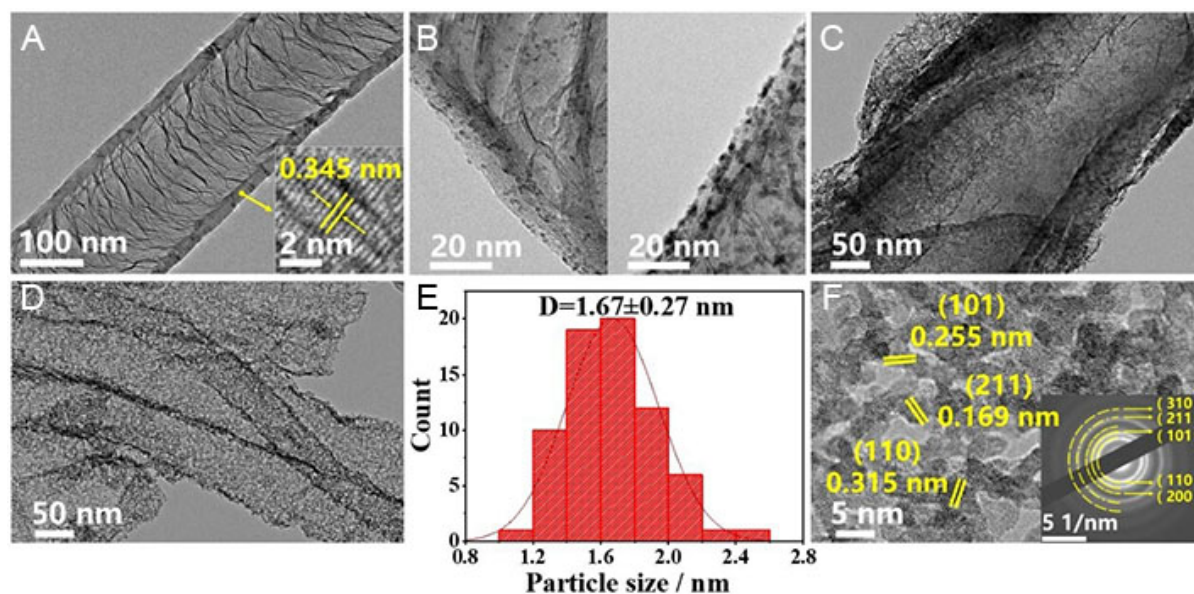


Figure 1. TEM characterization of CNT/Fe-Ni, CNT/Fe-Ni@RuO₂, CNT/Fe-Ni@RuO₂@PANI and CNT/Fe-Ni@RuO₂@PANI-350. TEM images of (A) CNT/Fe-Ni; (B) CNT/Fe-Ni@RuO₂ with low (left) and high (right) RuO₂ loading; (C) CNT/Fe-Ni@RuO₂@PANI, (D) CNT/Fe-Ni@RuO₂@PANI-350; (E) Particle size distribution histogram of CNT/Fe-Ni@RuO₂@PANI-350. (F) IFFT image of CNT/Fe-Ni@RuO₂@PANI-350, inset: corresponding SAED image.

species during the OER process. **Figure 1C** and **D** display a typical TEM image of CNT/Fe-Ni@RuO₂@PANI and CNT/Fe-Ni@RuO₂@PANI-350. The coating of PANI prevents the agglomeration of RuO₂ nanoparticles during high-temperature treatment. The TEM image of CNT/Fe-Ni@RuO₂@PANI-350 demonstrates the uniform distribution of RuO₂ nanoparticles which exhibit an average size of 1.67 ± 0.27 nm [Figure 1E]. The

high-resolution TEM image shown in [Figure 1F](#) reveals the high crystallinity of RuO₂ nanoparticles. The lattice spacing of 0.315, 0.255 and 0.169 nm corresponded to the (110), (101) and (201) crystal planes of the rutile-structured RuO₂. This observation aligns well with the selected-area electron diffraction (SAED) pattern shown in [Figure 1F](#), which exhibits distinct diffraction rings that are assigned to the (110), (101), and (211) planes of rutile RuO₂. These findings confirm the successful formation of RuO₂ NPs anchored on the CNT/Fe-Ni framework.

[Figure 2A](#) shows the XRD pattern of the CNT/Fe-Ni@RuO₂@PANI-350 sample. The sharp peak at 26.5° is the characteristic diffraction peak of (002) crystal plane of graphitic carbon (PDF# 75-1621), and the (110), (101) and (211) crystal planes of rutile RuO₂ (PDF# 71-2273) are also observed, further confirming the crystalline nature of the CNT as well as the presence of RuO₂. XPS measurements were conducted to obtain more structural information about the CNT/Fe-Ni@RuO₂@PANI-350 catalyst. Ru, Fe, Ni, O, C, and N elements were detected as shown in the survey XPS spectrum [[Figure 2B](#)]. [Supplementary Figure 5](#) displays the scanning transmission electron microscopy (STEM) and EDS elemental mapping images of the CNT/Fe-Ni@RuO₂@PANI-350 catalyst, demonstrating the uniform distribution of C, N, Fe, Ni throughout the CNT/Fe-Ni support as well as Ru and O from RuO₂ uniformly distributed on the CNT/Fe-Ni support. The N element was introduced from the acetonitrile precursor and PANI. The high-resolution C 1s and Ru 3d spectra are shown in [Figure 2C](#). The peak at a binding energy of 284.8 eV corresponds to the characteristic C=C bond in graphite, and the peak at a binding energy of 285.8 eV is attributed to C-N bonds in CNT/Fe-Ni@RuO₂@PANI-350. For the Ru 3d spectrum, the peaks at 281.1 and 285.4 eV correspond to Ru 3d_{5/2} and Ru 3d_{3/2} of RuO₂ with satellite peaks observed at 282.8 and 286.2 eV for Ru 3d_{5/2} and Ru 3d_{3/2}, respectively. The XPS spectra of Fe 2p and Ni 2p for CNT/Fe-Ni@RuO₂@PANI-350 [[Supplementary Figure 6](#)] are similar to those of CNT/Fe-Ni. The peaks centered at 705.5, 710.8/724.4 and 712.9/726.4 eV are assigned to Fe⁰, Fe²⁺ and Fe³⁺, respectively. The peaks centered at 850.6, 854.1 and 856.0 eV arise from Ni⁰, Ni²⁺ and Ni³⁺, respectively. The XPS analyses confirm the presence of Fe-Ni in the CNT/Fe-Ni@RuO₂@PANI-350 catalyst. [Figure 2D](#) displays the Ru 3p_{3/2} spectrum of CNT/Fe-Ni@RuO₂@PANI-350, featuring binding energies at 462.8 eV (Ru⁴⁺) and 465.3 eV (Ru³⁺). The presence of Ru³⁺ indicates the existence of oxygen vacancies (V_O) in RuO₂ NPs. In O 1s spectrum [[Figure 2E](#)], the peaks at binding energies of 529.7, 530.5, and 532.0 eV are associated with the lattice oxygen (O_L) in RuO₂, the oxygen in Ru-OH bond and C=O/C-O bonds, respectively. In addition, the peaks at 531.2 and 533.0 eV correspond to the oxygen adjacent to V_O and the surface-adsorbed oxygen-containing species, respectively. The formation of V_O in CNT/Fe-Ni@RuO₂@PANI-350 is attributed to the reaction between RuO₂ and carbon during the thermal treatment of CNT/Fe-Ni@RuO₂@PANI: RuO₂ + C → V_O-RuO₂ + CO₂^[38]. Besides, the synergistic effect between Fe-Ni and CNT can promote the formation of active sites^[39]. Therefore, the integration of defective RuO₂ with CNT/Fe-Ni is expected to promote the electrochemical performance of CNT/Fe-Ni@RuO₂@PANI-350. [Supplementary Figure 3B](#) displays the Raman spectra of both CNT/Fe-Ni@RuO₂@PANI-350 and CNT/Fe-Ni samples. It reveals that the CNT/Fe-Ni sample exhibits a lower graphitization degree. Carbon-based materials with reduced graphitization may contain more structural defects, which could increase the number of edge defects and provide additional growth sites for metal species^[40]. After heat treatment at 350 °C, CNT/Fe-Ni@RuO₂@PANI-350 shows a little increase in graphitization, compared with CNT/Fe-Ni. During the heat treatment at 350 °C, PANI underwent partial carbonization, and residual nitrogen species formed multiple types of active sites through doping, further enhancing the OER activity and stability of CNT/Fe-Ni@RuO₂@PANI-350 [[Figures 2F](#) and [3A](#)]. No significant Fe/Ni-related peaks are observed in the Raman spectra, likely due to the relatively low sensitivity of Raman spectroscopy to metallic phases. [Figure 2F](#) shows the N 1s spectrum of CNT/Fe-Ni@RuO₂@PANI-350, with characteristic binding energies of pyridinic N (398.2 eV), pyrrolic N (399.8 eV), graphitic N (400.9 eV), and oxidized N (402.1 eV). The analytical results of XPS calculations presented in [Supplementary Table 1](#) demonstrate that the relative weight percentage of RuO₂ in CNT/Fe-Ni@RuO₂@PANI-350 is 40.7 wt%.

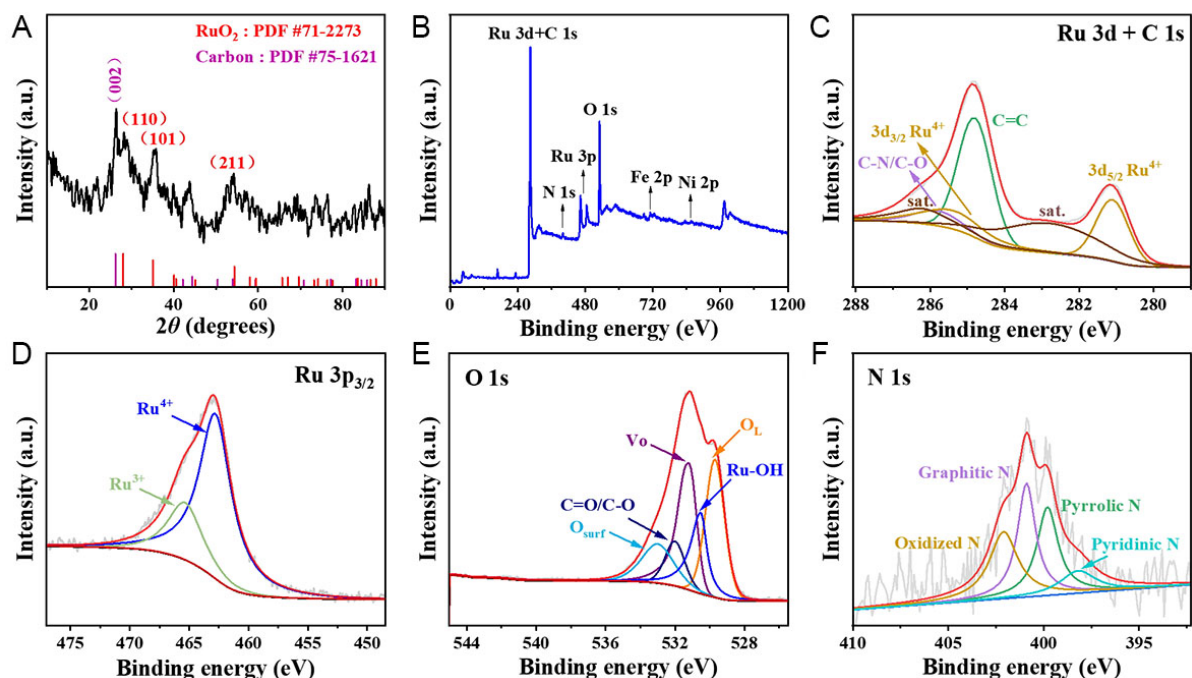


Figure 2. XRD and XPS characterization of CNT/Fe-Ni@RuO₂@PANI-350. (A) XRD pattern, (B) XPS survey spectrum, (C) Ru 3d and C 1s spectrum, (D) Ru 3p_{3/2} spectrum, (E) O 1s spectrum, and (F) N 1s spectrum.

Figure 3 illustrates the OER catalytic performance of CNT/Fe-Ni@RuO₂@PANI-350 in acidic conditions. Meanwhile, the OER catalytic performance of the catalyst prepared by only using ferrocene (denoted as CNT/Fe@RuO₂@PANI-350) or nickelocene (denoted as CNT/Ni@RuO₂@PANI-350) was also investigated for better comparison and to highlight the synergistic effect of Fe-Ni alloy. As shown in Figure 3A, CNT/Fe-Ni@RuO₂@PANI-350 exhibits the best OER activity, with an overpotential (η_{10}) of only ca. 188 mV at a current density of 10 mA cm⁻². The overpotential (η_{10}) of CNT/Fe-Ni@RuO₂@PANI-350 is significantly lower than those of CNT/Fe@RuO₂@PANI-350 (234 mV), CNT/Ni@RuO₂@PANI-350 (259 mV), and the other catalysts without PANI coating. The previous study has demonstrated that the catalysts with PANI modification exhibited better performance than the ones without PANI modification^[38]. As displayed in Figure 3B, the η_{10} values of CNT/Fe-Ni@RuO₂@PANI-350, CNT/Fe@RuO₂@PANI-350 and CNT/Ni@RuO₂@PANI-350 are lower than those of CNT/Fe-Ni@RuO₂-350, CNT/Fe@RuO₂-350 and CNT/Ni@RuO₂-350, respectively. This is potentially because the presence of PANI on the catalyst surface induces the formation of an ultra-thin carbon layer and abundant V_os in RuO₂ NPs during the calcination process, resulting in the improved catalytic activity of RuO₂. The corresponding Tafel plots shown in Figure 3C indicate that CNT/Fe-Ni@RuO₂@PANI-350 possesses the smallest Tafel slope of only 39.1 mV dec⁻¹. The Fe-C hetero-interface in CNT/Fe-Ni enhances the synergistic effect between metal and CNT, promoting the formation of active sites and improving catalytic activity^[41,42]. Furthermore, the catalytic activity can be further enhanced by the introduction of Ni. As indicated in Figure 3D, CNT/Fe-Ni@RuO₂@PANI-350 shows significantly improved OER catalytic activity compared with CNT/Fe@RuO₂@PANI-350. The overpotentials at the current density of 10 and 100 mA cm⁻² are reduced from 234 and 274 mV to 188 and 225 mV, respectively. Moreover, the catalytic activity of CNT/Fe-Ni@RuO₂@PANI-350 surpasses that of commercial RuO₂/CC (η_{10} = 310 mV), and most reported catalysts such as B-RuO₂ (η_{10} = 200 mV)^[43] and PtCo-RuO₂/C (η_{10} = 212 mV)^[44] as summarized in Supplementary Table 2. These results verify the superior OER activity of CNT/Fe-Ni@RuO₂@PANI-350 in acidic media. At a higher current density of 100 mA cm⁻² [Figure 3D], CNT/Fe-Ni@RuO₂@PANI-350 maintains a low overpotential (η_{100}) of 225 mV, which is significantly lower than those of

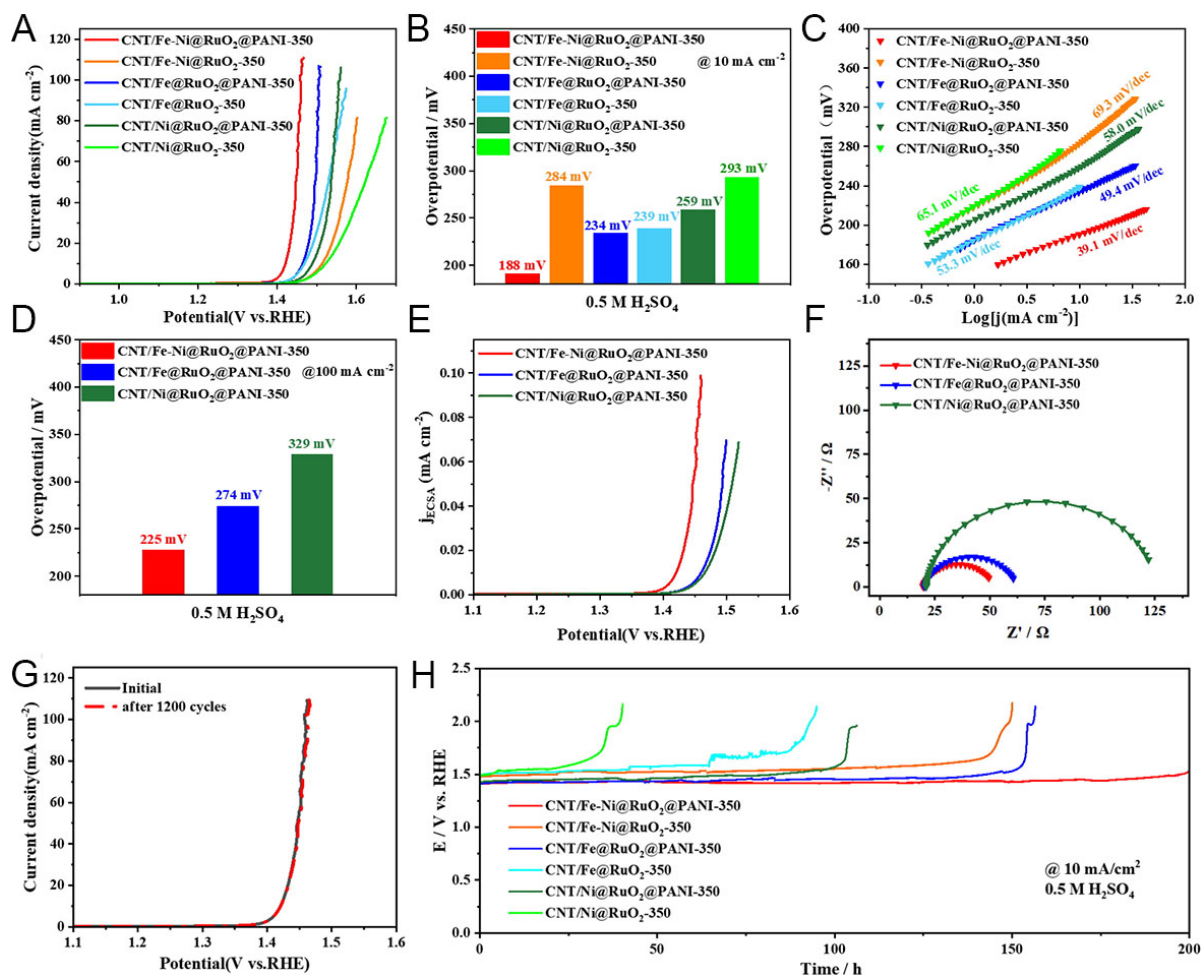


Figure 3. OER catalytic performance of different catalysts in 0.5 M H₂SO₄ solution. (A) OER polarization curves, (B) overpotentials at a current density of 10.0 mA cm⁻², (C) Tafel plots, (D) overpotentials at a current density of 100.0 mA cm⁻², (E) ECSA-normalized polarization profiles, (F) EIS spectra, (G) polarization profiles of CNT/Fe-Ni@RuO₂@PANI-350 before and after OER, (H) time-dependent potential curves.

CNT/Fe@RuO₂@PANI-350 ($\eta_{100} = 274$ mV) and CNT/Ni@RuO₂@PANI-350 ($\eta_{100} = 329$ mV). Such high-current performance is more favorable for practical applications, and the CNT/Fe-Ni@RuO₂@PANI-350 catalyst exhibits remarkable advantage at the increased current density. [Supplementary Figure 7](#) presents the OER catalytic performance of CNT/Fe-Ni, CNT/Fe-Ni@RuO₂, and CNT/Fe-Ni@RuO₂@PANI under acidic conditions. Combined with [Figure 3A](#), it reveals that samples without Ru loading or calcination treatment exhibit lower catalytic activity, demonstrating the necessity of both Ru loading and calcination treatment.

The intrinsic activity of CNT/Fe-Ni@RuO₂@PANI-350 towards the OER reaction is further evaluated by linear sweep voltammograms (LSVs) normalized by the ECSA. The ECSA of the catalyst can be calculated based on the C_{dl} value estimated by extrapolating the cyclic voltammograms (CVs) at different scan rates [[Supplementary Figure 8](#)]. The results show that the C_{dl} value of CNT/Fe-Ni@RuO₂@PANI-350 is 34.9 mF cm⁻², which is higher than those of CNT/Fe@RuO₂@PANI-350 (29.0 mF cm⁻²) and CNT/Ni@RuO₂@PANI-350 (13.8 mF cm⁻²). A higher C_{dl} value indicates a larger exposed area of the material in the electrolyte and more active sites, which is beneficial for improving the overall catalytic activity. The intrinsic activity evaluated by ECSA is proportional to the C_{dl} ($ECSA \propto C_{dl}$)^[44]. The ECSA of CNT/Fe-Ni@RuO₂

@PANI-350 calibrated by the formula is 70.5 cm^2 , higher than those of CNT/Fe@RuO₂@PANI-350 (58.6 cm^2) and CNT/Ni@RuO₂@PANI-350 (27.9 cm^2). The ECSA-normalized LSVs in Figure 3E show that the overpotential of CNT/Fe-Ni@RuO₂@PANI-350 is 190 mV to drive a current density of 0.01 mA cm^{-2} , which is lower than those of CNT/Fe@RuO₂@PANI-350 (230 mV) and CNT/Ni@RuO₂@PANI-350 (236 mV). These findings verify the higher intrinsic catalytic activity of CNT/Fe-Ni@RuO₂@PANI-350 towards OER. Moreover, CNT/Fe-Ni@RuO₂@PANI-350 demonstrates a reduced electrochemical impedance during OER, with a charge-transfer resistance of 31.8Ω , which is notably lower than those of CNT/Fe@RuO₂@PANI-350 (42.0Ω) and CNT/Ni@RuO₂@PANI-350 (104.5Ω), as shown in Figure 3F and Supplementary Figure 9. The lower charge transfer resistance indicates enhanced OER kinetics and an accelerated charge transfer rate in CNT/Fe-Ni@RuO₂@PANI-350. The high electrical conductivity is potentially attributed to the Fe-C strongly coupled interface, which affords an efficient electron transfer channel to enhance electron transfer efficiency^[42]. Additionally, CNT/Fe-Ni@RuO₂@PANI-350 also exhibits excellent durability for OER. As shown in Figure 3G, no noticeable decrease in activity is observed after 1,200 repeated OER cycles. The time-dependent OER test [Figure 3H] demonstrates that CNT/Fe-Ni@RuO₂@PANI-350 exhibits a minimal increase of $\sim 30 \text{ mV}$ in overpotential over 150 h reaction. In contrast, CNT/Ni@RuO₂-350, CNT/Fe@RuO₂-350, CNT/Ni@RuO₂@PANI-350, CNT/Fe-Ni@RuO₂-350 and CNT/Fe@RuO₂@PANI-350 lost their activities after working for 40, 94, 106, 150, and 156 h, respectively, during the OER stability test. This result demonstrates that the unique structural design of CNT/Fe-Ni@RuO₂@PANI-350 can protect RuO₂ NPs from chemical corrosion during the OER. Structural characterization in the Supplementary Figure 10 indicates that CNT/Fe-Ni@RuO₂@PANI-350 possesses excellent structural robustness. Even after undergoing 150 hours of OER testing, RuO₂ NPs are still clearly observable in the CNT/Fe-Ni@RuO₂@PANI-350 catalyst. The RuO₂ NPs exhibit no significant morphological changes in particle sizes [Supplementary Figure 11] and remain uniformly distributed on the CNT/Fe-Ni support [Supplementary Figure 12]. After the OER reaction in 0.5 M H₂SO₄ electrolyte, the CNT/Fe-Ni@RuO₂@PANI-350 catalyst exhibits no significant changes in morphological feature and element distribution [Supplementary Figure 12]. The unique structural design of CNT/Fe-Ni@RuO₂@PANI-350 demonstrates significant advantages in suppressing the leaching of Ru species. Consequently, the CNT/Fe-Ni@RuO₂@PANI-350 catalyst demonstrates outstanding catalytic activity and stability during the OER process. Notably, V_o in RuO₂ could still be identified in the Ru 3p and O 1s spectra [Supplementary Figure 13] of CNT/Fe-Ni@RuO₂@PANI-350. Spectral deconvolution reveals that the concentration of V_o in RuO₂ remains relatively stable during OER testing. The XRD pattern of CNT/Fe-Ni@RuO₂@PANI-350 after OER operation [Supplementary Figure 14] displays features comparable to those of the initial state. These observations strongly indicate the exceptional structural stability of CNT/Fe-Ni@RuO₂@PANI-350 in water electrolysis.

DFT simulation is further used to reveal the origin of catalytic activity and stability of the CNT/Fe-Ni@RuO₂@PANI-350 catalyst. Specifically, to simulate the CNT/Fe-Ni@RuO₂@PANI-350 composite structure, a Fe-Ni co-doped graphene supported RuO₂ (110) model (denoted as GPE/Fe-Ni@RuO₂) was constructed [Figure 4A]. In the computational model of GPE/Fe-Ni@RuO₂, Fe and Ni atoms are positioned adjacent to each other, representing the Fe-Ni alloy configuration. DFT calculations shown in Figure 4A reveal that the optimized Fe-O bond lengths at the interface of RuO₂ clusters combined with GPE/Fe-Ni and GPE/Fe are 1.737 and 1.740 Å, respectively, which are significantly shorter than those in FeO (2.166 Å) and Fe₂O₃ (1.983 Å). This finding suggests the formation of Fe-O chemical bonds at the interface between RuO₂ clusters and GPE/Fe-Ni or GPE/Fe. The RuO₂ (110) surface was selected because it is the most stable crystal plane of RuO₂^[45,46]. In this structural model, graphene (GPE) is used to simulate the carbon material. Calculation results show that the most stable adsorption configuration for RuO₂ loading is achieved in the GPE/Fe-Ni@RuO₂ model, with an adsorption energy of -5.57 eV. The adsorption energies for RuO₂ loading on GPE/Fe and GPE are -5.33 and -3.13 eV, respectively. This configuration of GPE/Fe-Ni@RuO₂ exhibits

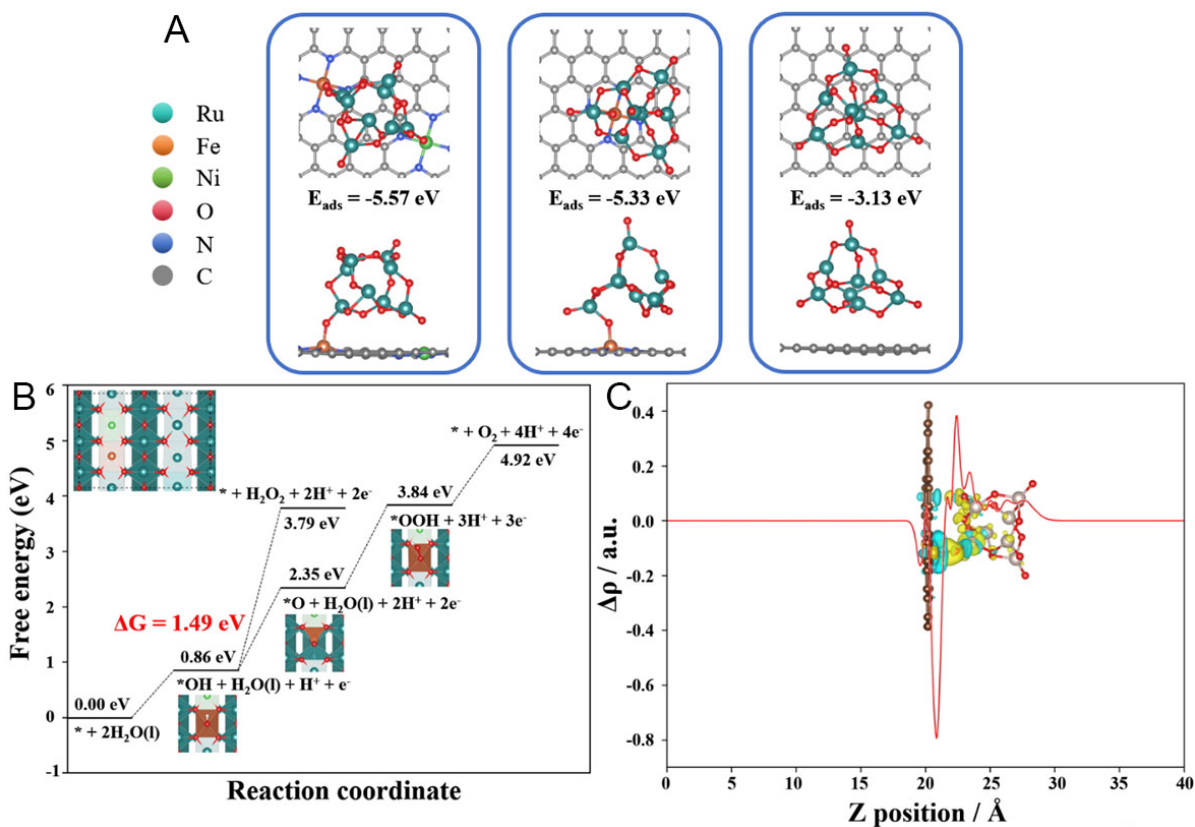


Figure 4. DFT simulations. (A) Optimized geometry of GPE/Fe-Ni@RuO₂, GPE/Fe@RuO₂, and GPE@RuO₂; (B) OER free energy diagram, (C) charge density difference analysis of GPE/Fe-Ni@RuO₂.

Fe-O and Ni-O interactions, confirming that the anchoring-confinement effect of Fe-Ni sites on the graphite surface significantly enhances the preferential loading of RuO₂. Notably, the RuO₂ (110) surface is exposed with a protonated oxygen-terminated form, which closely matches the distinct -OH characteristic peak observed in the O 1s spectrum of CNT/Fe-Ni@RuO₂@PANI-350. From a perspective view of thermodynamics, the more negative adsorption energy between GPE/Fe-Ni and RuO₂ demonstrates a stronger interaction, leading to the formation of a more stable structure. Furthermore, the calculations indicate that the OER active sites are the exposed Ru atomic sites on the RuO₂ (110) surface [Figure 4B]. The corresponding OER free energy diagrams reveal that for the GPE/Fe-Ni@RuO₂ system, both the *OH→*O and *O→*OOH conversions act as rate-determining steps, each exhibiting an energy barrier of 1.49 eV. In contrast, the rate-determining step shifts to the *OOH deprotonation process for both GPE/Fe@RuO₂ and GPE@RuO₂, with a higher energy barrier of 1.80 and 2.22 eV [Supplementary Figure 15], respectively. These theoretical calculations align well with the experimental results, elucidating the underlying mechanism responsible for the enhanced OER catalytic activity of CNT/Fe-Ni@RuO₂@PANI-350.

Charge density analysis was employed to reveal the influence of the catalyst's electronic structure on its OER activity^[47]. Figure 4C and Supplementary Figure 16 display the planar average charge density distribution curves of different catalyst models (GPE/Fe-Ni@RuO₂, GPE/Fe@RuO₂, and GPE@RuO₂). Significant charge redistribution is observed at the interface between RuO₂ (110) and graphite substrate under the synergistic effect of Fe-Ni bimetals [Figure 4C]. The yellow regions represent electron density depletion ($\Delta\rho < 0$), while cyan regions indicate electron density accumulation ($\Delta\rho > 0$). Local charge

integration analysis shows that the presence of Fe-Ni bimetals promotes directional charge transfer from RuO₂ to graphite substrate, resulting in a higher oxidation state of Ru sites. The results indicate that the distinct electronic interaction between RuO₂ and graphite substrate with the synergistic effect of Fe-Ni bimetals effectively enhances the oxidation capacity of RuO₂, thereby improving its OER catalytic performance^[48]. In contrast, the GPE@RuO₂ model exhibits minimal charge exchange between graphite substrate and RuO₂ clusters in absence of Fe-Ni or Fe. Such a difference in electronic interaction between RuO₂ and graphite substrate is closely related to the anchoring effect of Fe-Ni or Fe sites. Particularly, the planar average charge density curve of GPE/Fe-Ni@RuO₂ shows a sharper peak at the adsorption site for RuO₂, corresponding to the dual-site adsorption configuration induced by the Fe-Ni bimetallic sites. These findings at the electronic level corroborate the intrinsic mechanism that the anchoring-confinement effect of Fe-Ni bimetals on the CNT surface induces the preferential loading of RuO₂ and enhances its catalytic performance.

CONCLUSIONS

In conclusion, the RuO₂ nanoparticles decorated on Fe-Ni-doped CNTs have been prepared as a catalyst for OER in acidic conditions with high catalytic activity and stability. Experimental and theoretical investigations reveal that the nano-confinement effect induced by Fe-Ni bimetals on the CNT surface not only strengthens the anchoring stability of RuO₂ nanoparticles, but also promotes a significant increase in the oxidation state of active-site through interfacial electron coupling. These effects boost the catalytic activity of Ru sites and enhance the surface stability of Ru during OER. As a result, the catalyst exhibits a decent OER performance with overpotential of 188 and 225 mV at a current density of 10 and 100 mA cm⁻², respectively, in 0.5 M H₂SO₄. Notably, the catalyst sustains merely 30 mV overpotential increase throughout 150 h continuous operation at 10 mA cm⁻². This study proposes a bimetallic nano-confinement strategy addressing the stability of Ru-based catalysts, potentially opening an alternative way for designing OER electrocatalysts with both high activity and long-term stability.

DECLARATIONS

Authors' contributions

Conceptualization and supervision, review and editing: Zhao, Y.; Li, B.

Experimentation: Liu, S.; Tan, H.; Dai, G.

Investigation, methodology: Xiong, S.; Zhao, Y.; Li, B.

Materials characterization: Liu, S.; Dai, G.

Data analysis: Liu, S.; Tan, H.; Xiong, S.

Writing-original draft: Liu, S.

Availability of data and materials

All detailed materials and methods supporting the results of this study are included in the article/[Supplementary Materials](#). Further inquiries can be directed to the corresponding author(s).

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Conflicts of interest

All authors declared that there are no conflicts of interest.

Ethical approval and consent to participate

Not applicable.

Consent for publication

Not applicable.

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